## **Environmental Protection Agency**

 $E_p {=} emission \ rate \ of total fluorides from a potroom group, kg/Mg (lb/ton).$ 

C<sub>s</sub>=concentration of total fluorides, mg/dscm (gr/dscf).

 $Q_{sd}$ =volumetric flow rate of effluent gas, dscm/hr (dscf/hr).

P=aluminum production rate, Mg/hr (ton/hr). K=conversion factor, 106 mg/kg (7,000 gr/lb). 1=subscript for primary control system efflu-

1=subscript for primary control system effluent gas.

2=subscript for secondary control system or roof monitor effluent gas.

(2) The emission rate  $(E_b)$  of total fluorides from anode bake plants shall be computed for each run using the following equation:

 $E_b=(C_s Q_{sd})/(P_eK)$ 

where:

 $\begin{array}{ll} E_b {=} emission \ \ \, rate \ \ \, of \ \, total \ \, fluorides, \ \ \, kg/Mg \\ (lb/ton) \ \, of \ \, aluminum \ \, equivalent. \end{array}$ 

 $C_s$ =concentration of total fluorides, mg/dscm (gr/dscf).

 $Q_{sd} = volumetric$  flow rate of effluent gas, dscm/hr (dscf/hr).

 $P_e$ =aluminum equivalent for anode production rate, Mg/hr (ton/hr).

K=conversion factor, 106 mg/kg (7,000 gr/lb).

- (3) Methods 13A or 13B shall be used for ducts or stacks, and Method 14 for roof monitors not employing stacks or pollutant collection systems, to determine the total fluorides concentration ( $C_{\rm s}$ ) and volumetric flow rate ( $Q_{\rm sd}$ ) of the effluent gas. The sampling time and sample volume for each run shall be at least 8 hours and 6.80 dscm (240 dscf) for potroom groups and at least 4 hours and 3.40 dscm (120 dscf) for anode bake plants.
- (4) The monitoring devices of §60.194(a) shall be used to determine the daily weight of aluminum and anode produced.
- (i) The aluminum production rate (P) shall be determined by dividing 720 hours into the weight of aluminum tapped from the affected facility during a period of 30 days before and including the final run of a performance test.
- (ii) The aluminum equivalent production rate ( $P_e$ ) for anodes shall be determined as 2 times the average weight of anode produced during a representative oven cycle divided by the cycle time. An owner or operator may establish a multiplication factor other than 2 by submitting production records of the amount of aluminum produced and the

concurrent weight of anodes consumed by the potrooms.

(5) Method 9 and the procedures in §60.11 shall be used to determine opacity.

[54 FR 6669, Feb. 14, 1989, as amended at 65 FR 61757, Oct. 17, 2000]

## Subpart T—Standards of Performance for the Phosphate Fertilizer Industry: Wet-Process Phosphoric Acid Plants

# § 60.200 Applicability and designation of affected facility.

- (a) The affected facility to which the provisions of this subpart apply is each wet-process phosphoric acid plant having a design capacity of more than 15 tons of equivalent  $P_2O_5$  feed per calendar day. For the purpose of this subpart, the affected facility includes any combination of: reactors, filters, evaporators, and hot wells.
- (b) Any facility under paragraph (a) of this section that commences construction or modification after October 22, 1974, is subject to the requirements of this subpart.

[42 FR 37937, July 25, 1977, as amended at 48 FR 7129, Feb. 17, 1983]

#### § 60.201 Definitions.

As used in this subpart, all terms not defined herein shall have the meaning given them in the Act and in subpart A of this part.

- (a) Wet-process phosphoric acid plant means any facility manufacturing phosphoric acid by reacting phosphate rock and acid.
- (b) Total fluorides means elemental fluorine and all fluoride compounds as measured by reference methods specified in §60.204, or equivalent or alternative methods.
- (c) Equivalent  $P_2O_5$  feed means the quantity of phosphorus, expressed as phosphorus pentoxide, fed to the process.

[40 FR 33154, Aug. 6, 1975, as amended at 65 FR 61757, Oct. 17, 2000]

### § 60.202 Standard for fluorides.

(a) On and after the date on which the performance test required to be conducted by §60.8 is completed, no